



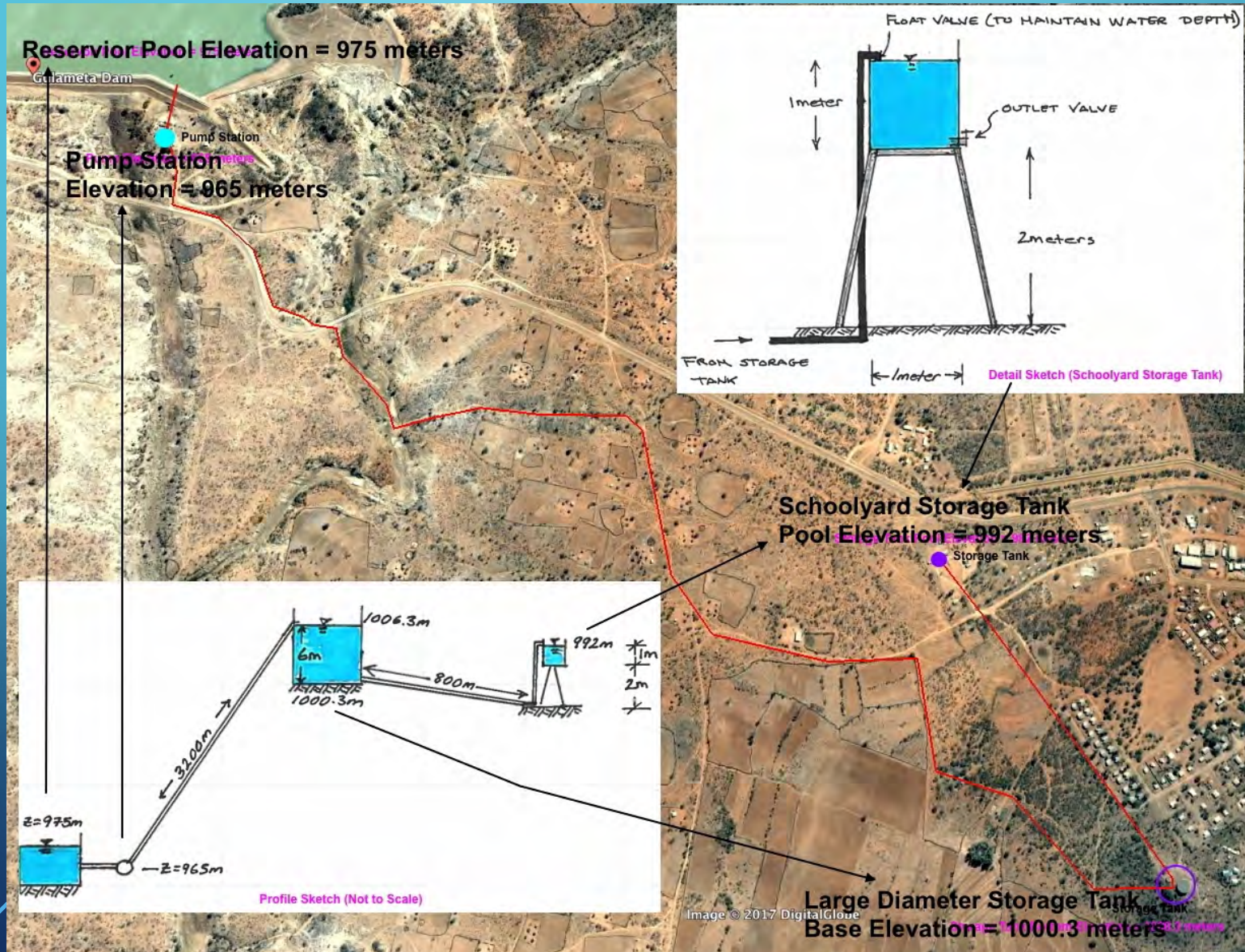
CE 3372 WATER SYSTEMS DESIGN

PIPELINE HYDRAULICS EXAMPLES : PART 3

LINKING SYSTEMS

- A hydraulic system can be analysed as a set of linked components to make an otherwise complicated system easier to analyze.
- Idea is to break system into independent parts, analyze the parts then reassemble to answer questions about the whole system
- Continued example

LINKING SYSTEMS

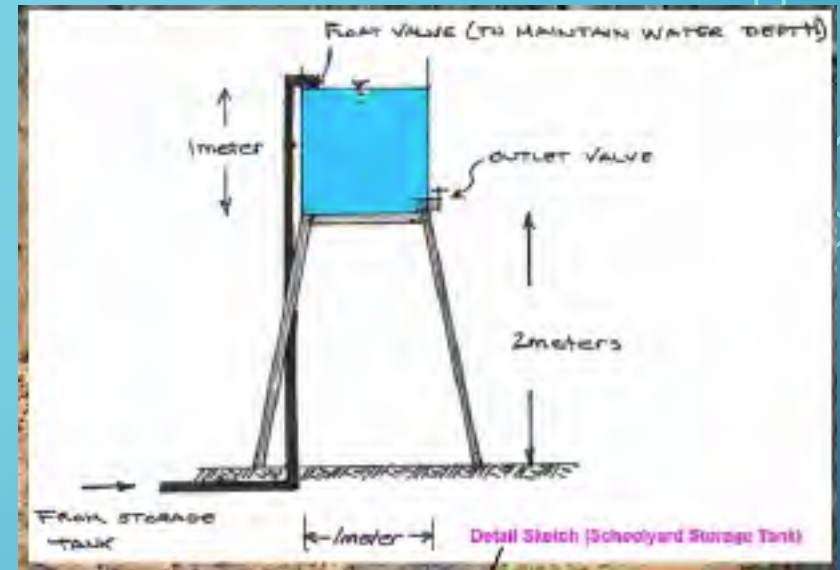


LINKING SYSTEMS

- Analyze proposed system to determine anticipated behavior
 - Float valve fails at school
 - Outlet valve accidently left open
 - Pump operation under worst failure mode
 - Pump fails, time until system fails
 - Float valve limited
 - Outlet valve limited

LINKING SYSTEMS

- Float valve fails at school



- Upstream head = 1006.3 m
(pump working, supply tank stays full)
- Downstream head = 992 m
(pool elevation at schoolyard tank overflow)

LINKING SYSTEMS

- Float valve fails at school
- $Z_1 = 1006.3 \text{ m}$; $Z_2 = 992 \text{ m}$
- 2 bends, $K = 1.5$ each
- 1 inlet $K = 0.5$
- Upstream valve $K = 0.15$
- Float valve $K = 70$
- Viscosity = 1.0 E-06 sq.m/s
- K_s (HDPE) = 0.007 mm
 0.000007 m



Water Properties (SI) using Python

Water Properties (SI)
adapted from Table A5 in Elger, Crowe, Roberson 2013. Engineering Fluid Mechanics. Wiley&Sons.

Machine Name : theodore-macbookpro.ttu.edu
Run Date : Tue Aug 11 14:54:11 2020

----- INPUT VALUES -----
Temperature = 20.0 (degrees C)
----- LOOKUP VALUES -----
Density = 998 (kg/m^3)
Specific Weight = 9790 (N/m^3)
Dynamic Viscosity = 0.001 (N-s/m^2)
Kinematic Viscosity = 1e-06 (m^2/s)
Vapor Pressure = 2340 (N/m^2) - absolute

Absolute Roughness Lookup using Python

Absolute Roughness Height (in millimeters) Lookup

Database Last Updated 10 AUG 2020

Machine name : atomickitty.ddns.net
Run Date : Tue Aug 11 14:48:16 2020

----- DATABASE QUERY VALUES -----
Description = PVC and plastic pipe
Absolute Roughness (millimeters) = 0.007
Reference = adapted from <https://www.nuclear-power.net/nuclear-engineering/fluid-dynamics/major-head-loss-friction-loss/relative-roughness-of-pipe/>

LINKING SYSTEMS

- Hydraulic Model

Discharge Between Two Reservoirs (SI Units)

Pipeline connecting two reservoirs. Pool elevations are Z1 and Z2.
 Pipeline length is L, diameter is D, sand roughness height is ks.
 Pipeline can be analyzed with entrance and exit loss coefficients (Ki and Ke).
 Pipeline can be analyzed with 2 fitting (Kf) loss coefficients.
 Calculator solves for flow rate in the pipeline.

Uses Jain equation to make initial flow estimate, then Newton's method to refine the estimate.

[Detailed Explanation](#) (Under Construction)

Pipeline Parameters	Fittings Parameters
Pool Elevation (Z1): 1006.3	Inlet Loss (Ki): 0.5
Pool Elevation (Z2): 992	Exit Loss (Ke): 70
Pipeline Length (L): 800	Fitting Loss (Kf): 0.15
Pipeline Diameter (D): 0.127	Fitting Loss (Kf): 3
Sand Roughness Height (ks): 0.000007	
Kinematic Viscosity (nu): 1e-6	
Gravitational Acceleration (g): 9.8	

Use zero fitting values to ignore minor losses

Discharge Between Two Reservoirs (SI units) (Update: 2020-0811)

Machine Name : atomickitty.ddns.net
 Run Date : Tue Aug 11 15:45:32 2020
 COMMAND TO RUN : /usr/bin/Rscript 2QReservoir.R

Return Code : 0

INPUT VALUES		
Pool Elevation 1 (Z1) =	1006.3	meters
Pool Elevation 2 (Z2) =	992.0	meters
Pipeline Length (L) =	800.0	meters
Pipeline Diameter (D) =	0.127	meters
Sand Roughness Height (ks) =	7e-06	meethers
Kinematic Viscosity (nu) =	1e-06	meters^2/second
Gravitational Acceleration (g) =	9.8	meters/second^2
Inlet Loss Coefficient (Ki) =	0.5	
Outlet Loss Coefficient (Ke) =	70.0	
Fitting Loss Coefficient (Kf) =	0.15	
Fitting Loss Coefficient (Kf) =	3.0	

COMPUTED RESULT		
Discharge =	0.01586378	m^3/sec
Friction Factor =	0.01667988	
EGL Slope =	0.017875	m/m

~ 16 liters/second

LINKING SYSTEMS

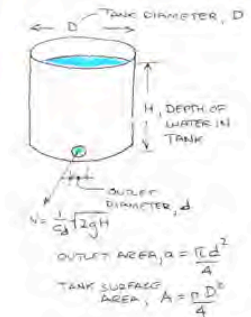
- Outlet valve left open
- Treat as hole in tank

Lesson Collection - Fall 2020 | Discharge from Circular Tank | JupyterLab

atomiccity.ddns.net/documents/mytoolbox

Flow-Rate Circular Tank

Compute Flow From a Tank



$v = \frac{1}{2} \sqrt{2gH}$
OUTLET AREA, $A = \frac{\pi d^2}{4}$
TANK SURFACE AREA, $A = \frac{\pi D^2}{4}$

d = Outlet pipe diameter
D = Tank diameter
H = Depth of water above outlet centerline
Cd = Discharge coefficient

Client-Side Javascript

----- INPUT VALUES -----

Outlet diameter (d in feet or meters)	0.05	
Tank Diameter (D in feet or meters)	1.00	
Depth (H in feet or meters)	1.00	
Discharge coefficient (Cd)	1	Use Cd=1 for Bernoulli Analysis
Gravitational acceleration (g)	9.8	SI=9.8, US=32.2
Submit Input Values		

----- COMPUTED RESULTS -----

Tank Pool Surface Area	0.7854	L ² (sq.ft. or sq.m.)
Outlet Area	0.0020	L ² (sq.ft. or sq.m.)
Discharge Rate	0.0087	L ³ /T (cfs or cms)

← ~ 8 liters/second

LINKING SYSTEMS

- Pump Requirements

- Float Valve Fails: $Q = 16$ LPS
- Outlet Valve Left Open: $Q = 8$ LPS
- Pipe Fails: $Q = 24$ LPS

- Thus a pump that produces

- $1006.3 - 975 = 29.3$ meters of head
- 24 LPS discharge should be suitable

- Example catalog listing next slide

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Return Code : 0

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Pipeline Diameter (D) =	0.127	meters
Sand Roughness Height (ks) =	7e-06	meethers
Kinematic Viscosity (nu) =	1e-06	meters^2/second
Gravitational Acceleration (g) =	9.8	meters/second^2
Inlet Loss Coefficient (Ki) =	0.5	
Outlet Loss Coefficient (Ke) =	70.0	
Fitting Loss Coefficient (Kf) =	0.15	
Fitting Loss Coefficient (Kf) =	3.0	

~ 16 liters/second

COMPUTED RESULT		
Discharge =	0.01586378	m^3/sec
Friction Factor =	0.01667988	
EGL Slope =	0.017875	m/m

Lesson Collection - Fall 2020 | Discharge from Circular Tank | JupyterLab

atommickitty.ddns.net/documents/mytoolbox=...

Flow-Rate Circular Tank

Compute Flow From a Tank

$d =$ Outlet pipe diameter
 $D =$ Tank diameter
 $H =$ Depth of water above outlet centerline
 $Cd =$ Discharge coefficient

Client-Side Javascript

----- INPUT VALUES -----

Outlet diameter (d in feet or meters)	0.05	
Tank Diameter (D in feet or meters)	1.00	
Depth (H in feet or meters)	1.00	
Discharge coefficient (Cd)	1	Use Cd=1 for Bernoulli Analysis
Gravitational acceleration (g)	9.8	SI=9.8, US=32.2
Submit Input Values		

----- COMPUTED RESULTS -----

Tank Pool Surface Area	0.7854	L ² (sq.ft. or sq.m.)
Outlet Area	0.0020	L ² (sq.ft. or sq.m.)
Discharge Rate	0.0087	L ³ /T (cfs or cms)

~ 8 liters/second

LINKING SYSTEMS

- Thus a pump that produces
 - 1006.3 – 975 = 29.3 meters of head
 - 24 LPS discharge should be suitable
 - E.g. Kirloskar KLS 1537 specified for 100mm pipe, so will need reducer/expander
- However when we analyze the pumping side, don't have the correct pump
 - Can only produce 7 LPS , because we forgot the pipe friction.
 - Options?
 - 2 in series

Lesson Collection - Fall 2020 Discharge Between Two Reservoirs JupyterLab

Machine Name : theodore-macbookpro.ttu.edu
 Run Date : Mon Sep 7 20:46:58 2020
 COMMAND TO RUN : /usr/bin/Rscript 2QReservoirWithPump.R

Return Code : 0

INPUT VALUES			
Pool Elevation 1 (Z1) =	975.0	meters	
Pool Elevation 2 (Z2) =	1006.3	meters	
Pipeline Length (L) =	3200.0	meters	
Pipeline Diameter (D) =	0.127	meters	
Sand Roughness Height (ks) =	7e-06	meters	
Kinematic Viscosity (nu) =	1e-06	meters^2/second	
Gravitational Acceleration (g) =	9.8	meters/second^2	
Inlet Loss Coefficient (Ki) =	0.5		
Outlet Loss Coefficient (Ke) =	1.0		
Fitting Loss Coefficient (Kf) =	2.55		
Fitting Loss Coefficient (Kf) =	0.32		
Pump Shutoff Head (Hp@Q_0) =	40.0	Discharge (Q_0)	0.0
Pump Point One (Hp@Q_1) =	30.0	Discharge (Q_1)	0.028
Pump Point Two (Hp@Q_2) =	14.0	Discharge (Q_2)	0.036

←←← Fittings at pump

COMPUTED RESULT		
Discharge =	0.0076394	m^3/sec ←
Added Head =	40.35164	m
Friction Losses =	9.051641	m
Static Lift =	31.3	m
Pipeline Friction Factor =	0.01918692	
Fitted Pump Shutoff =	41.48688	m
Pump Constant =	-19452.23	m/Q^2

LINKING SYSTEMS

- Thus a pump that produces
 - 1006.3 – 975 = 29.3 meters of head
 - 24 LPS discharge should be suitable
 - E.g. Kirloskar KLS 1537 specified for 100mm pipe, so will need reducer/expander
- However when we analyze the pumping side, don't have the correct pump
 - Can only produce 7 LPS , because we forgot the pipe friction.
 - Options?
 - 2 in series (Almost works)
 - Probably look for a bigger pump, but for grins, lets try 3 in series

Machine Name : theodore-macbookpro.ttu.edu
 Run Date : Mon Sep 7 20:53:15 2020
 COMMAND TO RUN : /usr/bin/Rscript 2QReservoirWithPump.R
 Return Code : 0

INPUT VALUES			
Pool Elevation 1 (Z1) =	975.0	meters	
Pool Elevation 2 (Z2) =	1006.3	meters	
Pipeline Length (L) =	3200.0	meters	
Pipeline Diameter (D) =	0.127	meters	
Sand Roughness Height (ks) =	7e-06	meters	
Kinematic Viscosity (nu) =	1e-06	meters^2/second	
Gravitational Acceleration (g) =	9.8	meters/second^2	
Inlet Loss Coefficient (Ki) =	0.5		
Outlet Loss Coefficient (Ke) =	1.0		
Fitting Loss Coefficient (Kf) =	2.55		
Fitting Loss Coefficient (Kf) =	0.32		
Pump Shutoff Head (Hp@Q_0) =	80.0	Discharge (Q_0)	0.0
Pump Point One (Hp@Q_1) =	60.0	Discharge (Q_1)	0.028
Pump Point Two (Hp@Q_2) =	28.0	Discharge (Q_2)	0.036

COMPUTED RESULT		
Discharge =	0.01734215	m^3/sec
Added Head =	71.27324	m
Friction Losses =	39.97324	m
Static Lift =	31.3	m
Pipeline Friction Factor =	0.01641738	
Fitted Pump Shutoff =	82.97376	m
Pump Constant =	-38904.47	m/Q^2

LINKING SYSTEMS

- Thus a pump that produces
 - 1006.3 – 975 = 29.3 meters of head
 - 24 LPS discharge should be suitable
 - E.g. Kirloskar KLS 1537 specified for 100mm pipe, so will need reducer/expander
- However when we analyze the pumping side, don't have the correct pump
 - Can only produce 7 LPS , because we forgot the pipe friction.
 - Options?
 - 3 in series (essentially working)
 - But best look for a bigger pump

Machine Name : theodore-macbookpro.ttu.edu
 Run Date : Mon Sep 7 20:55:39 2020
 COMMAND TO RUN : /usr/bin/Rscript 2QRReservoirWithPump.R
 Return Code : 0

INPUT VALUES			
Pool Elevation 1 (Z1) =	975.0	meters	
Pool Elevation 2 (Z2) =	1006.3	meters	
Pipeline Length (L) =	3200.0	meters	
Pipeline Diameter (D) =	0.127	meters	
Sand Roughness Height (ks) =	7e-06	meters	
Kinematic Viscosity (nu) =	1e-06	meters^2/second	
Gravitational Acceleration (g) =	9.8	meters/second^2	
Inlet Loss Coefficient (Ki) =	0.5		
Outlet Loss Coefficient (Ke) =	1.0		
Fitting Loss Coefficient (Kf) =	2.55		
Fitting Loss Coefficient (Kf) =	0.32		
Pump Shutoff Head (Hp@Q_0) =	120.0	Discharge (Q_0)	0.0
Pump Point One (Hp@Q_1) =	90.0	Discharge (Q_1)	0.028
Pump Point Two (Hp@Q_2) =	42.0	Discharge (Q_2)	0.036

COMPUTED RESULT		
Discharge =	0.02240409	m^3/sec
Added Head =	95.16888	m
Friction Losses =	63.86888	m
Static Lift =	31.3	m
Pipeline Friction Factor =	0.0157098	
Fitted Pump Shutoff =	124.4606	m
Pump Constant =	-58356.7	m/Q^2