# CE 3372 WATER SYSTEMS DESIGN

PIPELINE HYDRAULICS EXAMPLES : PART 2

- A hydraulic system can be analysed as a set of linked components to make an otherwise complicated system easier to analyze.
- Idea is to break system into independent parts, analyze the parts then reassemble to answer questions about the whole system
- Best illustrated by an example



- Analyze proposed system to determine anticipated behavior
  - Float valve fails at school
  - Outlet valve accidently left open
  - Pump operation under worst failure mode
  - Pump fails, time until system fails
    - Float valve limited
    - Oultet valve limited





• Upstream head = 1006.3 m

(pump working, supply tank stays full)

Downstream head = 992 m
(pool elevation at schoolyard tank overflow)

- Float valve fails at school
- $Z_1 = 1006.3 \text{ m}$ ;  $Z_2 = 992 \text{ m}$
- 2 bends, K =1.5 each
- 1 inlet K = 0.5
- Upstream valve K = 0.15
- Float valve K = 70
- Viscosity = 1.0 E-06sq.m/s
- Ks (HDPE) = 0.007mm 0.000007m

2=975m -B=9455	ni Brothe Sherich (Pet to Scale)	20m tim 2m
•••• < > 🗉	Not Secure - atomickitty.ddns	5 🖞 🗗
M	Water Properties (SI) using Python	+
Machine Name : theodore-n Run Date : Tue Aug 11 14:5 INPUT VALUES Temperature = 20.0 (degrees LOOKUP VALUES Density = 998 (kg/m <sup>3</sup> 3) Specific Weight = 9790 (N/n Dynamic Viscosity = 0.001 Kinematic Viscosity = 1e-00 Vapor Pressure = 2340 (N/n	nacbookpro.ttu.edu (4:11 2020 s C) (N-s/m^2) 5 (m^2/s) 1^2) - absolute	* fit =
	Absolute Bouldhoose Lookup (c) - Suite	
Absolute Roughness Height	(in millimeters) Lookup	
Database Last Updated 10 A Machine name : atomickitty, Run Date : Tue Aug 11 14:4 DATABASE QUERY Description = PVC and plast Absolute Roughness (millim Reference = adapted from ht dynamics/major-head-loss-fr	UG 2020 ddns.net 8:16 2020 VALUES tic pipe teters) = 0.007 tps://www.nuclear-power.net/nuclea riction-loss/relative-roughness-of-pip	r-engineering/fluid- pe/

#### • Hydraulic Model

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#### **Discharge Between Two Reservoirs (SI Units)**



Pipeline connecting two reservoirs. Pool elevations are Z1 and Z2. Pipeline length is L, diameter is D, sand roughness height is ks. Pipeline can be analyzed with entrance and exit loss coefficients (Ki and Ke). Pipline can be analyzed with 2 fitting (Kf) loss coefficients. Calculator solves for flow rate in the pipeline.

Uses Jain equation to make initial flow estimate, then Newton's method to refine the estimate.

#### Detailed Explaination (Under Construction)

Pipeline Parameters
Pool Elevation (Z1):
1006.3
Pool Elevation (Z2):
992
Pipeline Length (L) :
Pipeline Diameter (D) :
0.127
Sand Roughness Height (ks) : 0.000007
Kinematic Viscosity (nu) :
1e-6
Gravitational Acceleration (g)
9.8
9.8

Fittings Parameters
Inlet Loss (Ki):
0.5
Exit Loss (Ke) :
70
Fitting Loss (Kf) :
0.15
Fitting Loss (Kf) :
3

Use zero fitting values to ignore minor losses

M	Disc	harge Between Two Reservoirs	(SI units)(Update: 2020-0811)
Machine Name : atomickitty.ddns.n Run Date : Tue Aug 11 15:45:32 20 COMMAND TO RUN : /usr/bin/Rs Return Code : 0	et 20 script 2QReser	voir.R	
INPUT VALUES			
Pool Elevation 1 (Z1) =	1006.3	meters	
Pool Elevation 2 (Z2) =	992.0	meters	
Pipeline Length (L) =	800.0	meters	
Pipeline Diameter (D) =	0.127	meters	
Sand Roughness Height (ks) =	7e-06	meethers	
Kinematic Viscosity (nu) =	1e-06	meters^2/second	
Gravitational Acceleration (g) =	9.8	meters/second^2	
Inlet Loss Coefficient (Ki) =	0.5		
Outlet Loss Coefficient (Ke) =	70.0		
Fitting Loss Coefficient (Kf) =	0.15		
Fitting Loss Coefficient (Kf) =	3.0	4	
	×5	TEL ANTH	
COMPUTED RESULT			
Discharge =	0.0158637	8 m^3/sec	
Friction Factor =	0.0166798	5	

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