

SCRIPT

ENERGY IS A MEASURE OF ABILITY TO DO WORK.

EXAMPLES:

- WATER STORED IN A DAM
- WIND ACROSS A PROPELLER
- GASOLINE BURNED IN A CYLINDER TO PUSH AGAINST A PISTON

BOARD

ENERGY CONCEPTS

ENERGY IS A PROPERTY THAT QUANTIFIES THE ABILITY TO DO WORK



SPRING LIFTS W, x UNITS —  
ENERGY STORED IN SPRING IS Wx

SCRIPT

KINDS OF ENERGY

MECHANICAL ENERGY —

ENERGY ASSOCIATED WITH MOTION OR POSITION IN A FORCE FIELD.

THERMAL ENERGY —

ENERGY ASSOCIATED WITH  $\Delta T$  AND/OR PHASE CHANGE

CHEMICAL ENERGY

CHEMICAL KE BONDS BREAKING RELEASE OR USE ENERGY

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UNITS OF ENERGY ARE:

JOULE =  $1N \cdot 1m$

$1ft \cdot 1lb = 1ft \cdot lb$

POWER IS ENERGY/TIME

$\frac{1N \cdot m}{s}$

$\frac{1ft \cdot lb}{s}$



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ELECTRICAL ENERGY

ENERGY ASSOCIATED WITH ELECTRICAL CHARGE IN AN ELECTRICAL FIELD

NUCLEAR ENERGY

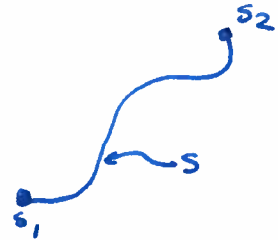
ENERGY ASSOCIATED WITH RADIOACTIVE DECAY

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WORK

$$W = F \cdot d$$

$$= \int_{s_1}^{s_2} F \cdot ds$$



Force (vector) applied through path  $s$  is work.

POWER

$$\frac{\text{WORK}}{\text{TIME}}$$

$$P = \frac{F \cdot d}{t} = F \cdot v$$

THIS IS VELOCITY

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TYPICAL "POWER"

LAPTOP COMPUTER, DISPLAY ON; FANS ON IS ABOUT 100W OR 100 J/s

WELL CONDITIONED SOLDIER CAN PRODUCE 300 J/s FOR AN HOUR OR TWO ~ 600W·hr OR 0.6 kW·hr WILL BURN OVER 2000 calories

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ENERGY IN FLUID SYSTEMS:

- COMPRESSION = PRESSURE
- ELEVATION = "POTENTIAL"
- MOMENTUM = "KINETIC"

EXTRACTING ENERGY

- TURBINES
  - WATER (LIQUID)
  - AIR (GAS)

ADDING ENERGY

- PUMPS
  - LIQUIDS
- COMPRESSORS
  - GAS

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THERMODYNAMICS  
IDEAS ARE  
FUNDAMENTAL  
TO ENERGY CONCEPT

• WORK

• HEAT TRANSFER

CONSIDER A BALLOON.

PUT NEXT TO HEAT  
LAMP -

TEMP ↑

P ↑

PUSHES AGAINST  
RUBBER WALLS,

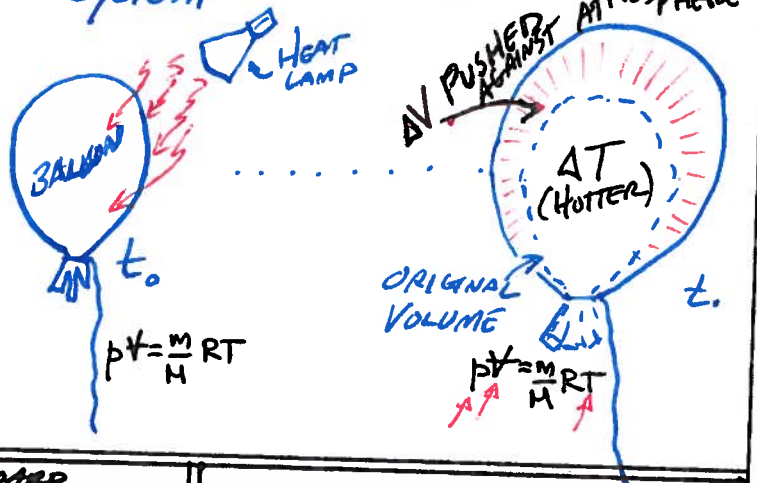
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ENERGY BALANCE

$$\Delta E = \dot{Q} - \dot{W}$$

↑ HEAT TRANSFER INTO SYSTEM  
 ↓ WORK DONE BY SYSTEM

CHANGE IN  
ENERGY STORED  
IN SYSTEM



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THE BALLOON EXPANDS,  
PUSHES AGAINST  
ATMOSPHERE.

$F \cdot d \Rightarrow$  DID WORK

∴ ΔE ↑ BECAUSE  
Q ↑. SOME ΔE  
LOST BECAUSE  
BALLOON HAD TO  
PUSH AGAINST  
ATMOSPHERE (W)

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AS A RATE EXPRESSION THE  
1<sup>ST</sup> LAW OF THERMODYNAMICS  
IS

$$\frac{dE}{dt} = \frac{d\dot{Q}}{dt} - \frac{d\dot{W}}{dt}$$

THESE ARE OFTEN  
WRITTEN AS

$$\frac{dE}{dt} = \dot{Q} - \dot{W}$$



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Now Apply REYNOLD'S  
 TRANSPORT THEOREM

$e$  IS INTENSIVE  
 PROPERTY  $\frac{E}{M}$ .

$U$  IS INTERNAL  
 ENERGY; IT IS  
 COMPRISED OF  
 "PRESSURE" + CHEMICAL;  
 NUCLEAR; ELECTRICAL;  
 ENERGY

"PRESSURE" IS STRONGLY  
 TEMPERATURE DEPENDENT

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$$\left. \frac{dQ}{dt} - \frac{dW}{dt} \right|_{\text{sys}} = \frac{d}{dt} \int_{\text{C.V.}} \rho e \, dV + \int_{\text{C.S.}} \rho e \vec{V} \cdot d\vec{A}$$

$e$  - ENERGY PER UNIT MASS

$$e = e_k + e_{\text{pot.}} + U$$

$U$  = INTERNAL ENERGY (ENERGY A  
 SUBSTANCE POSSESSES BY  
 STATE OF MOLECULAR ACTIVITY)

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IN "U":

FLOW WORK  
 (AT A SECTION IS  
 DIAGRAMED pg 258)

BOARD

$$\frac{dQ}{dt} = \dot{Q} = \text{HEAT TRANSFER INTO}$$

~~SYSTEM~~ C.V.

$$\frac{dW}{dt} = \dot{W} = \text{WORK DONE BY C.V.}$$

FLOW WORK

$$\text{WORK} = F \cdot d \quad \therefore dW = F dx$$

$$\text{THUS } \frac{dW}{dt} = F \frac{dx}{dt} = F \cdot V$$

(DIMENSIONALLY A POWER!)



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$p$  IS PRESSURE  
 AT SECTION ①

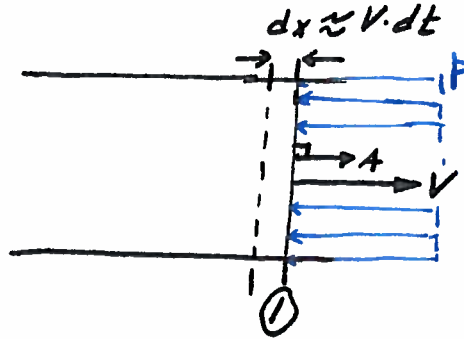
$V$  IS VELOCITY  
 AT SECTION ①

$A$  IS OUTWARD POINT  
 AREA VECTOR

$dx$  IS SMALL REGION  
 JUST AS GET TO ①  
 $dx \approx v \cdot dt$

RELATE PRESSURE FORCE  
 TO MOMENTUM

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CONSIDER MOMENTUM AT ①

$$F_p = \int_{c.s.} \vec{v} \cdot \rho \vec{v} \cdot d\vec{A}$$

$$pA = \rho V^2 A$$

DISTANCE THE FORCE APPLIED IS  
 $dx = v dt$

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NOW APPLY THIS  
 FORCE THROUGH  $dx$   
 TO FIND WORK  
 THE FLOW DOES  
 AT SECTION ①

SO WHEN APPLY  
 FORCE TO  $dx$  IN  
 TERMS  $dx = v dt$

FIND THAT

$$\dot{W} = pQ = \rho V^2 Q$$

$Q$  IS DISCHARGE  
 (HERE IS UNFORTUNATE

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$$\therefore F_p dx = pA v dt = \rho V^2 A \cdot v dt$$

THUS

$$\dot{W} = F_p \frac{dx}{dt} = pAV = \rho V^2 AV$$

↑  
 $v$

SO

$$F \cdot v = \underbrace{pAV}_Q = \rho V^2 \underbrace{AV}_Q = \dot{W}$$

(DISCHARGE)

CASE WHERE  $Q = \text{DISCHARGE}$   
 $\dot{Q} = \text{HEAT FLOW}$



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USUALLY FLOW  
WORK IS INCORPORATED  
INTO THE FLUX  
INTEGRAL

NOW USE THESE  
TERMS IN  
ENERGY EQUATION

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$$\int_{c.s.} \rho \left( \frac{p}{\rho} + e \right) \vec{v} \cdot d\vec{A}$$

NOW CONSIDER 2 FORMS

$$e_k = \frac{\text{KINETIC ENERGY}}{\text{MASS}} = \frac{mv^2}{2m} = \frac{v^2}{2}$$

$$e_p = \frac{\text{GRAVITATIONAL ENERGY}}{\text{MASS}} = \frac{mgz}{m} = gz$$

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NOTE THE  
FLOW WORK  
IS IN THE INTEGRAL  
 $\dot{W}_s$  IS "SHAFT"  
WORK

- ITS A SUPERFLY  
THING!

- FLOW WORK REPRESENTS THE ENERGY REQUIRED FOR THE FLUID TO FLOW AGAINST PRESSURE FORCES (BACK PRESSURE)
- SHAFT WORK REPRESENTS ENERGY THAT CAN BE REMOVED BY MECHANICAL DEVICES FROM THE FLOW FIELD AND PUT TO USE

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$$\dot{Q} - \dot{W}_s = \frac{d}{dt} \int_{c.v.} \rho \left( \frac{v^2}{2} + gz + u \right) dV$$

$$+ \int_{c.s.} \rho \left( \frac{p}{\rho} + \frac{v^2}{2} + gz + u \right) \vec{v} \cdot d\vec{A}$$



SCRIPT

APPLICATION OF  
 CONCEPT

DRAW C.V., C.S.

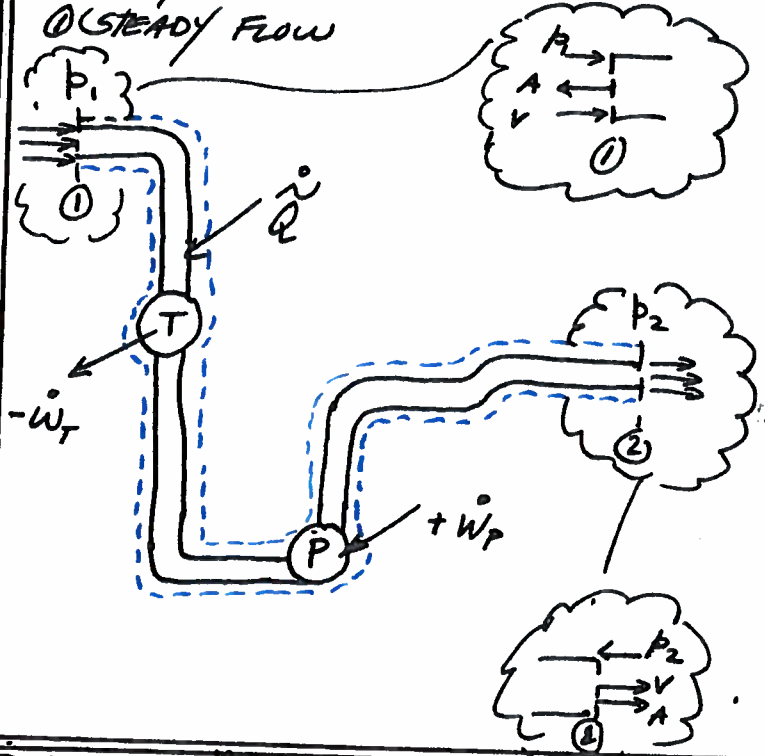
NOTE  $p, v, A$   
 AT INLETS/OUTLETS

WRITE ENERGY  
 BALANCE

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ENERGY IN A PIPELINE

① STEADY FLOW



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OBSERVE THAT

$$\dot{W}_S = \dot{W}_P - \dot{W}_T$$

NOW EVALUATE THE  
 FLUX INTEGRALS

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$$\dot{Q} - \dot{W}_S = \frac{d}{dt} \int_{C.V.} \left( \frac{v^2}{2} + gz + u \right) \rho dV$$

0 (steady flow)

$$+ \int_{①} \left( \frac{p_1}{\rho} + gz_1 + \frac{v_1^2}{2} + u_1 \right) \rho \vec{v} \cdot d\vec{A}$$

$$+ \int_{②} \left( \frac{p_2}{\rho} + gz_2 + \frac{v_2^2}{2} + u_2 \right) \rho \vec{v} \cdot d\vec{A}$$



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INTEGRAL AT SECTION  
 ① IS

~~2~~

INTEGRAL AT  
 SECTION ② IS :


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$$\int_{\text{①}} \frac{p_1}{\rho} \cdot \rho \vec{v} \cdot d\vec{A} + \int_{\text{①}} \rho g z_1 \vec{v} \cdot d\vec{A} + \int_{\text{①}} \rho \frac{v_1^2}{2} \vec{v} \cdot d\vec{A} + \int_{\text{①}} \rho u_1 \vec{v} \cdot d\vec{A}$$

$$\int_{\text{②}} \frac{p_2}{\rho} \rho \vec{v} \cdot d\vec{A} + \int_{\text{②}} \rho g z_2 \vec{v} \cdot d\vec{A} + \int_{\text{②}} \rho \frac{v_2^2}{2} \vec{v} \cdot d\vec{A} + \int_{\text{②}} \rho u_2 \vec{v} \cdot d\vec{A}$$

SCRIPT

USE FLOW DIAGRAM TO EVALUATE SIGN  $\vec{v} \cdot d\vec{A}$

INTRODUCE KINETIC ENERGY CORRECTION COEFFICIENTS WHICH RELATE K.E. DISTRIBUTED ACROSS  $v(r)$   TO AN AVERAGE (MEAN SECTION VELOCITY)

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$$= -\frac{p_1}{\rho} \rho Q - g z_1 \rho Q - \frac{\alpha_1 v_1^2}{2} \rho Q - u_1 \rho Q + \frac{p_2}{\rho} \rho Q + g z_2 \rho Q + \frac{\alpha_2 v_2^2}{2} \rho Q + u_2 \rho Q$$

$\alpha_1$  &  $\alpha_2$  ARE KINETIC ENERGY CORRECTION FACTORS

$$\int \rho \frac{v^2}{2} \vec{v} \cdot d\vec{A} \quad \bar{v}_1 = \frac{\int v \cdot dA}{\int dA}$$

$$= \int \frac{\rho}{2} v^3 dA_1 = \frac{\rho}{2} \int v^3 dA_1 = \frac{\rho}{2} \alpha_1 \int \bar{v}_1^3 dA$$

$$\therefore \alpha_1 = \frac{\int v^3 dA}{\bar{v}_1^3 \int dA}$$





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TYP. VALUES  $\alpha$

$$1 \leq \alpha \leq 2$$



LAMINAR

TURBULENT

DIVIDE BY  $g$   
AND REARRANGE  
EQUATION

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RESULT IS

$$\dot{Q} + \dot{w}_p - \dot{w}_t = \frac{p_1}{\gamma} Q - g z_1 \gamma Q - \alpha_1 \frac{V_1^2}{2} \gamma Q - u_1 \gamma Q$$

$$+ \frac{p_2}{\gamma} Q + g z_2 \gamma Q + \alpha_2 \frac{V_2^2}{2} \gamma Q + u_2 \gamma Q$$

REARRANGE AND DIVIDE BY  $g$

$$\frac{\dot{w}_p}{\gamma Q g} + \frac{p_1}{\gamma g} + \frac{g z_1 + \alpha_1 V_1^2}{g} = \frac{p_2}{\gamma g} + \frac{g z_2 + \alpha_2 V_2^2}{g}$$

ADDED HEAD (PUMP)

REMOVED HEAD (TURBINE)

HEAD LOSS

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OBSERVE DIMENSIONS  
ARE LENGTH.

THEY ARE CALLED  
"HEAD"

THEY REPRESENT  
ENERGY PER UNIT  
WEIGHT OF FLUID

BOARD

(TURBINE)

USUALLY THIS LAST EXPRESSION IS  
WRITTEN (AND MEMORIZED) AS

$$\frac{p_1}{\gamma} + \frac{\alpha_1 V_1^2}{2g} + z_1 + h_p = \frac{p_2}{\gamma} + \frac{\alpha_2 V_2^2}{2g} + z_2 + h_t + h_L$$

NOTICE THE REMARKABLE SIMILARITY  
TO BERNOULLI'S EQUATION!

EXAMINE COMMON NAMES FOR EACH  
TERM

$$\frac{p}{\gamma} \rightarrow \text{"PRESSURE HEAD"}$$



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THE EXPRESSION  
IS VALID FOR  
STEADY, ONE-DIMENSIONAL  
(AXIAL), INCOMPRESSIBLE  
FLOW IN A PIPE

IN ABSENCE OF  
FRICTIONAL LOSSES  
AND HEAT TRANSFER  
 $h_L = 0$   
(INVISCID FLOW)

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$$\frac{\alpha V^2}{2g} \rightarrow \text{"VELOCITY HEAD"}$$

( $\alpha$  IS USUALLY UNITY  
IN MANY PRACTICAL FLOW)

$$z \rightarrow \text{"ELEVATION HEAD"}$$

$$\frac{p}{\gamma} + z \rightarrow \text{"STATIC HEAD"}$$

$$\frac{p}{\gamma} + z + \frac{\alpha V^2}{2g} \rightarrow \text{"TOTAL HEAD"}$$

"TOTAL DYNAMIC HEAD"

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THIS IS A FUNDAMENTAL  
TOOL IN HYDRAULICS

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EXAMPLE

A PUMP DRAWS WATER FROM RESERVOIR A  
AND LIFTS IT TO A HIGHER RESERVOIR B.

THE HEAD LOSS FROM A TO THE PUMP  
IS 4 TIMES THE VELOCITY HEAD.

THE HEAD LOSS FROM THE PUMP TO  
B IS ~~SEVEN~~ 7 TIMES THE VELOCITY  
HEAD IN THE PIPE. FIND THE  
PRESSURE HEAD THE PUMP  
MUST DELIVER IF PRESSURE  
AT THE PUMP SUCTION INLET IS  
-6M OF WATER.



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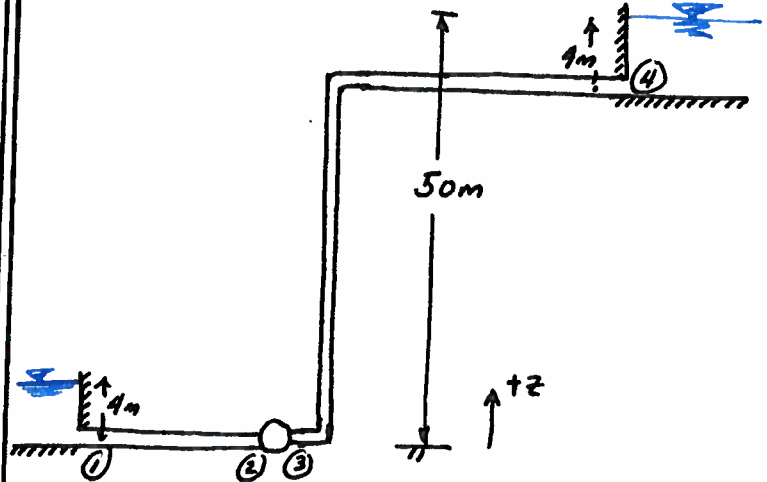
APPLY ENERGY EQUATION  
FROM ① → ②

THEN ③ → ④

USE CONTINUITY  
AS NEEDED.

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SKETCH; WITH VARIOUS ELEVATIONS



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ENERGY ① → ②

$$h_1 + h_p = h_2 + h_T + h_L$$

0 NO PUMP  
BETWEEN 1 & 2

0 NO TURBINE  
BETWEEN 1 & 2

EXPAND EXPRESSIONS FOR WHAT'S LEFT

$$h_1 = \frac{p_1}{\gamma} + \frac{V_1^2}{2g} + z_1 \quad ; \quad h_2 = \frac{p_2}{\gamma} + \frac{V_2^2}{2g} + z_2$$

$$h_L = \frac{4V^2}{2g}$$

CONTINUITY

$$V = V_1 = V_2 \quad (\text{CONSTANT DIAMETER PIPE})$$

$$\therefore \frac{p_1}{\gamma} + \frac{V^2}{2g} + z_1 = \frac{p_2}{\gamma} + \frac{V^2}{2g} + z_2 + \frac{4V^2}{2g}$$



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$$\frac{p_1}{\gamma} = \frac{p_2}{\gamma} + \frac{4V^2}{2g} \quad \frac{p_1}{\gamma} = 4m$$

$$\frac{p_2}{\gamma} = -6m$$

SO

$$\left(\frac{p_1 - p_2}{\gamma}\right) \frac{2g}{4} = V^2$$

$$V = \sqrt{\frac{(10m)(2)(9.8m/s^2)}{4}} = 7m/s$$

ENERGY FROM (3) → (4)

$$\frac{p_3}{\gamma} + \frac{V_3^2}{2g} + z_3 + h_p = \frac{p_4}{\gamma} + \frac{V_4^2}{2g} + z_4 + h_f + h_L$$

= 0      No Pumps 3 → 4      = 0 No TURB. 3 → 4

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$V_3 = V_4$  CONSTANT DIAMETER PIPE

∴

$$\frac{p_3}{\gamma} = \frac{p_4}{\gamma} + z_4 + h_L \quad h_L = \frac{7V^2}{2g}$$

$$\frac{p_3}{\gamma} = \frac{p_4}{\gamma} + z_4 + \frac{7V^2}{2g}$$

$$z_4 = 50m \quad \frac{p_4}{\gamma} = 4m$$

$$h_L = \frac{7(7)^2}{2g} = 17.5m$$

$$\therefore \frac{p_3}{\gamma} = 4m + 50m + 17.5m = 71.5m$$



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ENERGY ② → ③ (ACROSS PUMP)

$$\frac{p_2}{\gamma} + \frac{v_2^2}{2g} + z_2 + h_p = \frac{p_3}{\gamma} + \frac{v_3^2}{2g} + z_3 + h_f + h_L$$

= 0 No TURBS.

ASSUME  $v_2 \approx v_3$

ASSUME  $h_L$  IN  
MACHINE IS NEGLIGIBLE  
(ITS NOT, BECOMES  
PART MACHINE  
EFFICIENCY)

$$\frac{p_2}{\gamma} + h_p = \frac{p_3}{\gamma}$$

$$h_p = \frac{p_3}{\gamma} - \frac{p_2}{\gamma} = 71.5\text{m} - (-6\text{m})$$

$$= 77.5\text{m}$$

↑ ADDED HEAD REQUIRED  
BY THE PUMP

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BOARD

HGL & EGL  
(Pg 273-277)

HYDRAULIC & ENERGY GRADE LINES

$$\frac{p_1}{\gamma} + z_1 + \frac{v_1^2}{2g}$$

← STATIC HEAD →

← TOTAL HEAD →

THE HYDRAULIC GRADE LINE (HGL)  
IS AN IMAGINARY LINE THAT CONNECTS  
THE STATIC HEAD IN THE SYSTEM  
ITS HEIGHT REPRESENTS THE "STATIC"  
ENERGY OF THE SYSTEM AT SOME  
POINT.



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THE ENERGY GRADE LINE IS AN IMAGINARY LINE THAT CONNECTS TOTAL HEAD IN THE SYSTEM.

• ITS HEIGHT REPRESENTS TOTAL ENERGY OF THE SYSTEM AT SOME POINT.

HGL = HYDRAULIC GRADE-LINE  
EGL = ENERGY GRADE LINE

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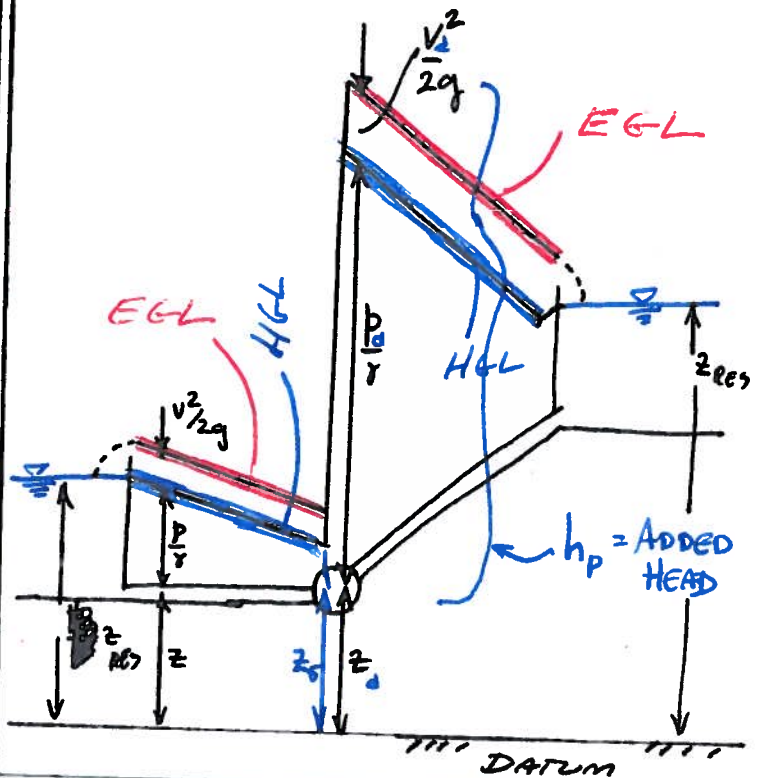
DRAWING

$$HGL = \frac{P}{\gamma} + z \text{ (BLUE)}$$

$$EGL = HGL + \frac{V^2}{2g} \text{ (RED)}$$

ADDED HEAD IS

$$\frac{p_d}{\gamma} + \frac{V_d^2}{2g} - \frac{p_s}{\gamma} - \frac{V_s^2}{2g} = h_p$$





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DRAWING HGL/EGL

- ① HEAD LOSS IN SYSTEM IMPLIES HGL SLOPES DOWNWARD IN DIRECTION OF FLOW.
- ② A PUMP ADDS TOTAL HEAD TO A SYSTEM SO THE EGL JUMPS
- ③  $\frac{p}{\gamma} = 0$  HGL = WATER LINE
- ④  $\frac{p}{\gamma} < 0$  POSSIBLE CAVITATION (pg 191)

CAVITATION DESCRIBED  
 PG 191

SCRIPT

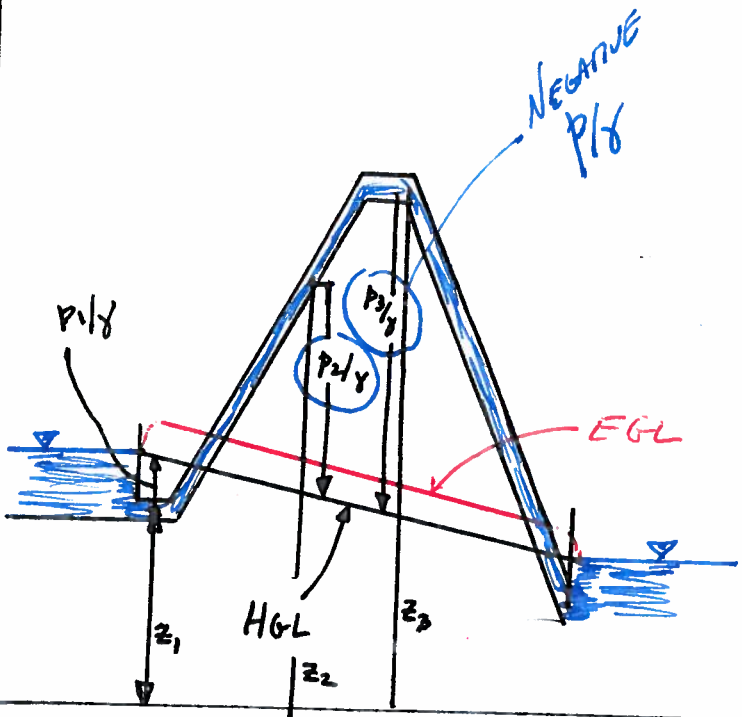
BOARD

IMPORTANCE OF  
 NEGATIVE PRESSURE  
 DEPENDS ON  
 WORKING FLUID

FOR WATER

$$\frac{p}{\gamma} < -10m$$

THEN ARE CLOSE TO  
 VAPOR PRESSURE  
 AND WILL FORM  
 VAPOR BUBBLES,  
 WHICH IS BAD. —  
 LIKE CROSSING THE  
 BEAMS (GHOST BUSINES)





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GOOD EXERCISES

- 7.25
- 7.34
- 7.40
- 7.48
- 7.56
- 7.61
- 7.87
- 7.82

DO 4x4

7.25
7.34
7.40
7.48
7.56
7.61
7.82
7.87

↓ SUBSET

↓

GOOD EXAM QUESTIONS

- 7.29
- 7.78 + SUBSET EXERCISES

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