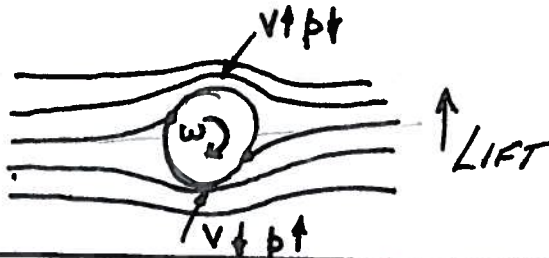
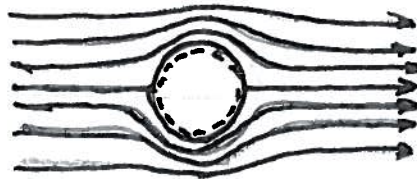


LIFT

Property called
circulation

Integral of tangential velocities
around a surface - if
any asymmetry, then "circulation"
If circulation, slight imbalances
of pressure force \Rightarrow lift

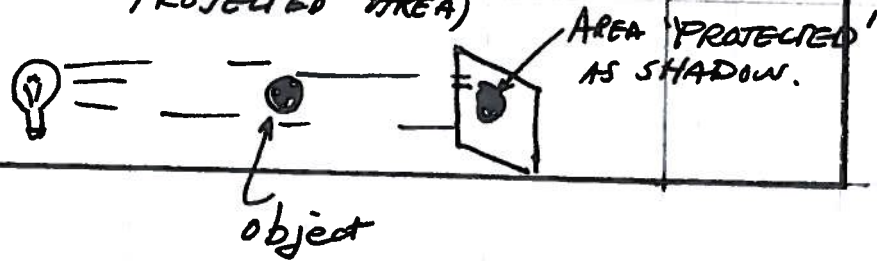
LIFT



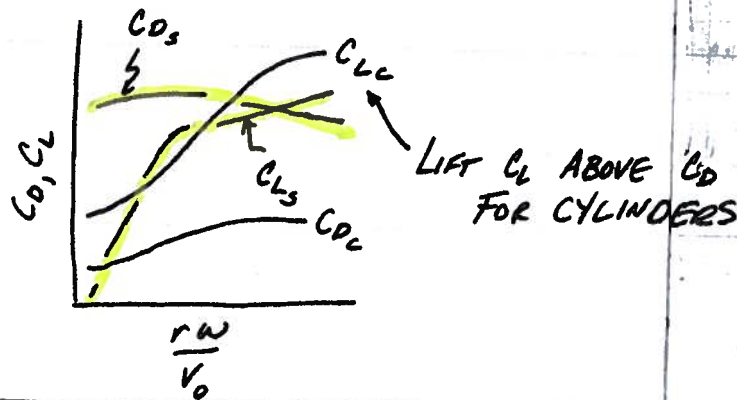
AS WITH DRAG

$$C_L = \frac{F_L}{A \left(\rho \frac{V_0^2}{2} \right)}$$

REFERENCE AREA (USUALLY PROJECTED AREA)



FOR SPINNING CYLINDERS/SPHERES
Ω MATTERS



EXAMPLE 11.6 p 425 GOOD ILLUSTRATION
HOW TO USE CHARTS



AIRFOILS (AND PROPELLER BLADES)



WHEN INTEGRATE, OBTAIN ASYMMETRIC
TANGENTIAL v ,
HENCE LIFT.

AIRFOIL THEORY ELABORATE,
NOTICE ~~THE~~ SIGNIFICANT
ESTIMATOR OF LIFT & DRAG ARE
ANGLE OF ATTACK





Terminal Velocity (Stokes Flow)

$$F_B = \gamma_w V$$

$$F_D = C_D A_P \frac{\rho V^2}{2}$$



$$W = \gamma_s V$$

Force balance

$$F_D + F_B = W$$

$$\frac{C_D A_P \rho V^2}{2} + V \gamma_w = \gamma_s V$$

← SOLVE FOR V

$$C_D A_P \rho \frac{V^2}{2} (\gamma_s - \gamma_w) V$$

$$\frac{V^2}{2} = \frac{(\gamma_s - \gamma_w) V}{C_D A_P \rho}$$

$$V = \left[\frac{2(\gamma_s - \gamma_w) V}{C_D A_P \rho} \right]^{1/2}$$



$$A_p = \frac{\pi d^2}{4}$$

$$V = \frac{A d^3}{6}$$

$$V = \left[\frac{2(\gamma_s - \gamma_w) \frac{\pi d^3}{6}}{\frac{\pi d^2}{4} C_D \rho} \right]^{1/2}$$

$$V^* = \left(\frac{(\gamma_s - \gamma_w)(4/3)d}{C_D \rho} \right)^{1/2}$$

$$C_D \propto \frac{V_0 d}{V}$$

↑
Re

i.e. FOR VALUES
IN EXAMPLE 11.4

THEN BUILD TABLE

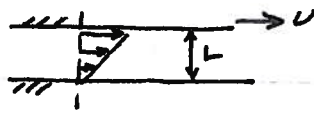
V	Re	C _D	V*
1 m/s	20,000	0.456	0.413
0.413	8264	0.406	0.438
⋮	⋮	⋮	⋮
⋮	⋮	⋮	⋮
⋮	⋮	⋮	⋮



LAMINAR FLOW & BOUNDARY LAYERS
CHAPTER 9

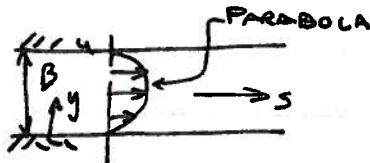
p 326-327

Couette Flow



$$\gamma = N \frac{U}{L} \quad (\text{WE DID SIMILAR ANALYSIS BACK IN CHAP. 3})$$

Hele-Shaw Flow

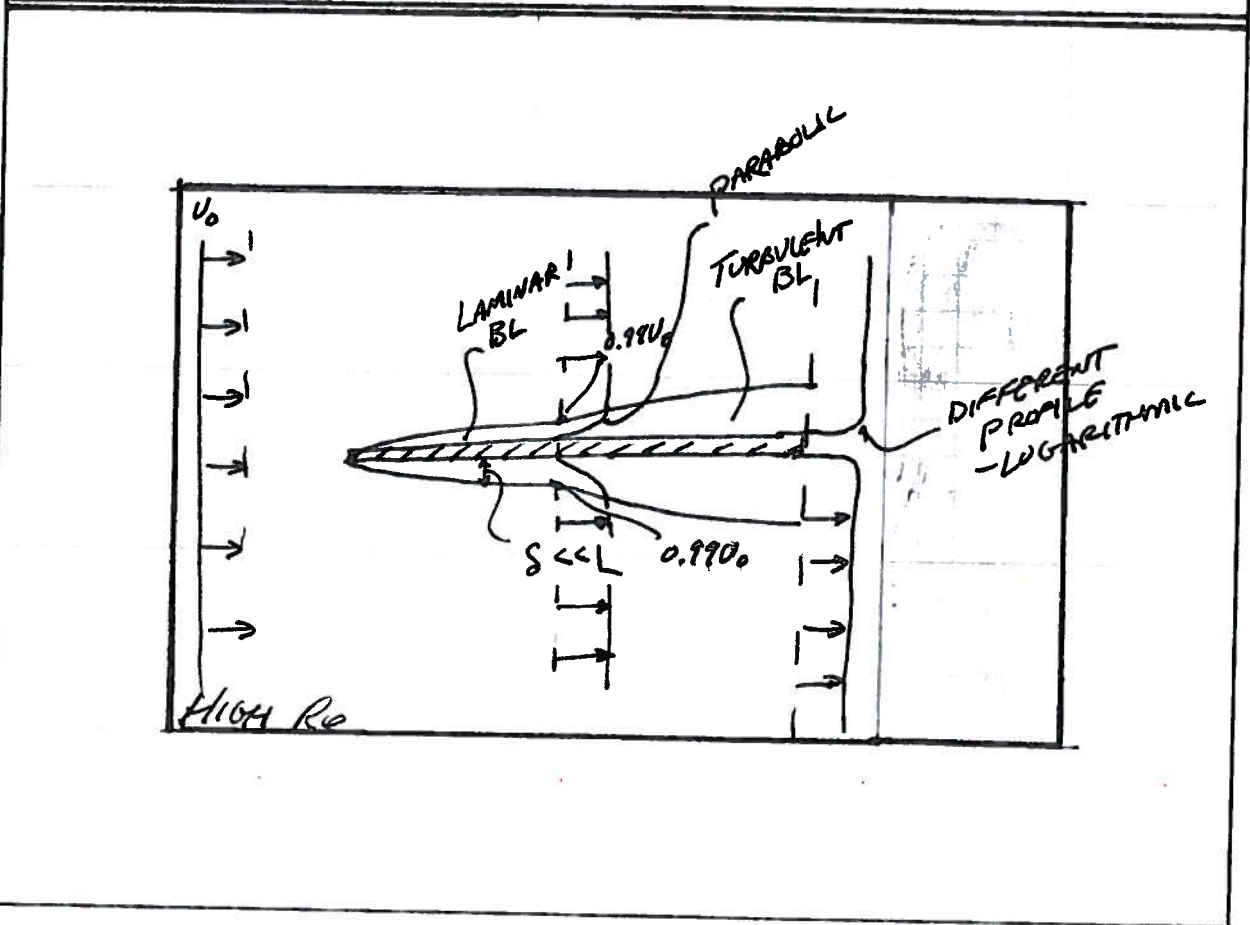
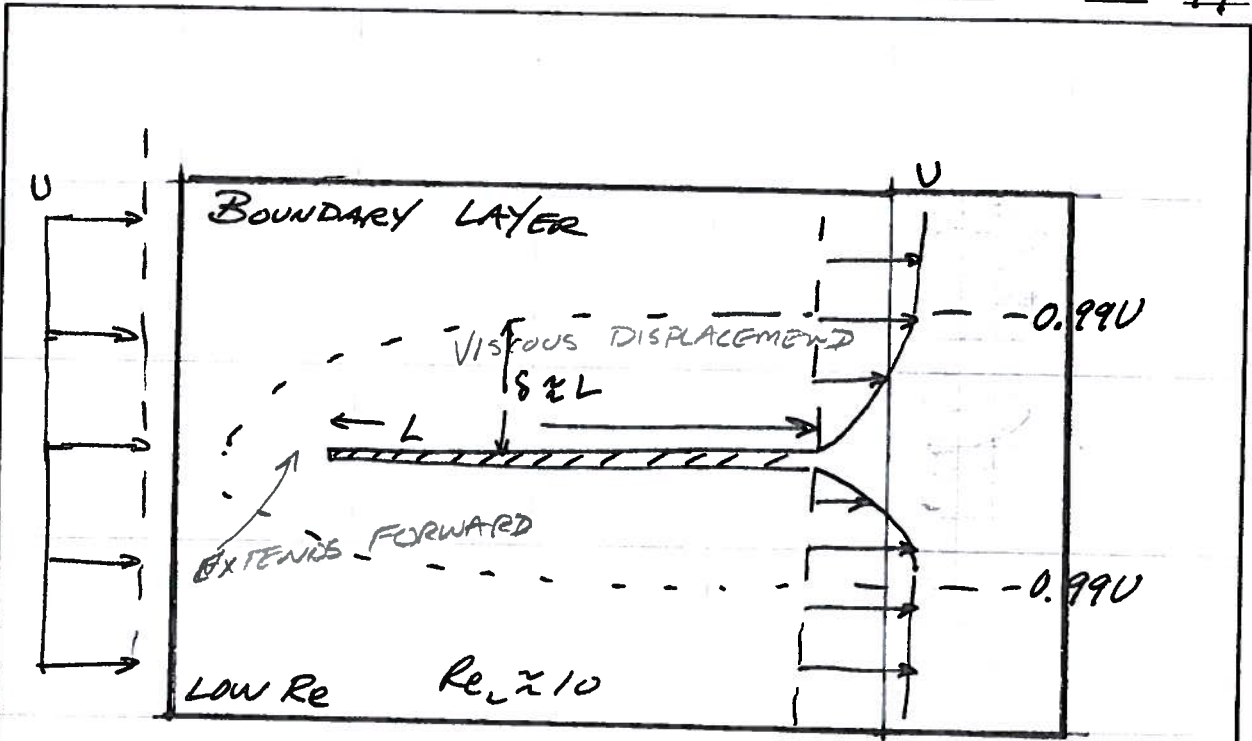


$$u = -\frac{1}{2\mu} (B^2 - y^2) \frac{d(p+\rho z)}{ds}$$

$$\bar{v} = \frac{2}{3} u_{\max}$$

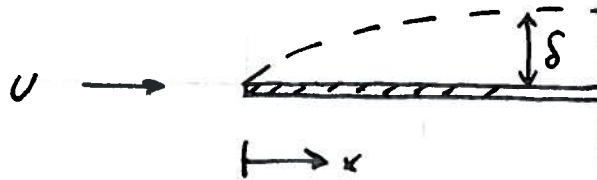
(GOOD APPROXIMATION FOR POROUS FLOW)

p 328





Blasius' approximation for BL thickness



Laminar

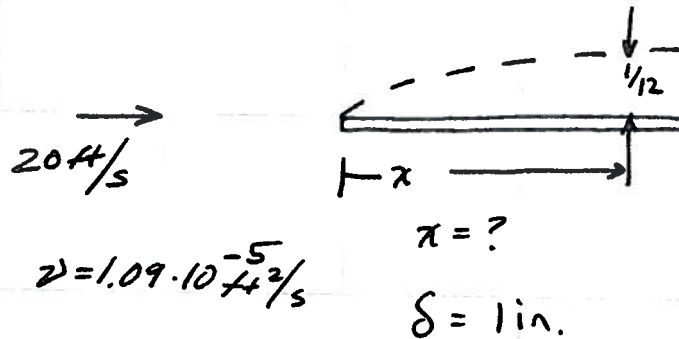
$$\delta = \frac{5x}{Re_x^{1/2}} \quad (Re_x < 10^6)$$

Turbulent

$$\delta = \frac{0.16x}{Re_x^{1/7}} \quad (Re_x > 10^6)$$



Suppose situation below:



Assume laminar

$$Re_x = \frac{Ux}{\nu}$$

$$\frac{U}{\nu} = \frac{20 \text{ ft/s}}{1.09 \cdot 10^{-5} \text{ ft}^2/\text{s}} = 1.84 \cdot 10^6 \text{ ft}^{-1}$$



$$\delta = \frac{5x}{\sqrt{1.84 \cdot 10^6 x}} \quad \text{SOLVE FOR } x$$
$$\delta = \frac{1}{2}$$

$$\delta^2 = \frac{25x^2}{1.84 \cdot 10^6 x}$$
$$\frac{1.84 \cdot 10^6 \left(\frac{1}{2}\right)^2}{25} = 511 \text{ ft}$$

Check Re_x

$$Re_x = 1.84 \cdot 10^6 \cdot 511 \text{ ft} = 9.4 \cdot 10^8 > 10^6$$

\therefore NOT LAMINAR,
USE TURBULENT
MODEL (EQ 9.32)



$$\delta = \frac{0.16 x}{(Re_x)^{1/7}}$$

$$\delta = \frac{0.16 x}{(1.84 \cdot 10^6 x)^{1/7}}$$

$$\delta^7 = \frac{(0.16)^7 (x)^7}{1.84 \cdot 10^6 x} = \frac{(0.16)^7 (x)^6}{1.84 \cdot 10^6}$$

$$\frac{\delta^7 \cdot 1.84 \cdot 10^6}{(0.16)^7} = x^6$$

$$x = \left[\frac{\delta^7 (1.84 \cdot 10^6)}{(0.16)^7} \right]^{1/6}$$

$$= \left[\frac{(1/2)^7 (1.84 \cdot 10^6)}{(0.16)^7} \right]^{1/6} = 5.17 \text{ ft}$$

$$Re_x = \frac{(20)(5.17)}{1.09 \cdot 10^{-5}} = 9.5 \cdot 10^6 > 10^6 \text{ TURBULENT}$$

\therefore AT GIVEN CONDITIONS,
B.L. = 1 in AT 5.17 ft FROM LEADING
EDGE.



Utility of BL is to estimate shear force on plate.

Once shear force is known drag from plate can be approximated. Used for guiding experiments, forcing layer transition to control drag

Shear force (one side) drag

$$C_f = \frac{F_s}{A \left(\frac{\rho V_o^2}{2} \right)}$$

$$C_f = \frac{1.33}{Re_x^{1/2}} \quad (\text{LAMINAR})$$

$$C_f = \frac{0.032}{Re_x^{1/2}} \quad (Re < 10^7); \quad \frac{0.523}{\ln^2(0.06 Re_x)}$$

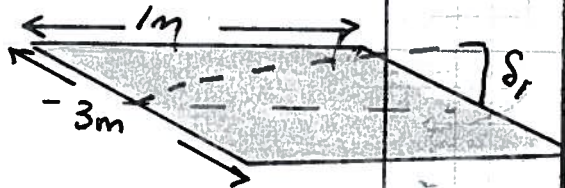


Consider plate

$$V = 2 \text{ m/s}$$

$$\rho = 1.23 \text{ kg/m}^3$$

$$\nu = 1.46 \cdot 10^{-5} \text{ m}^2/\text{s}$$



FIND δ AT TRAILING EDGE

FIND DRAG ON ONE SIDE OF PLATE

$$Re_L = \frac{(2.0)(1.0)}{1.46 \cdot 10^{-5}} = 137,000 < 10^6$$

LAMINAR.

$$C_f = \frac{1.33}{(137,000)^{1/2}} = 0.0036$$

$$F_s = C_f A \left(\frac{\rho V_0^2}{2} \right)$$

$$= (0.0036)(3)(1)(1.23)(2)^2 \left(\frac{1}{2} \right) = 0.0265 \text{ N}$$

\uparrow m \uparrow m \uparrow kg/m³ \uparrow m/s

$$\frac{\text{kg m}^4}{\text{m}^3 \cdot \text{s}^2} = \frac{\text{kg m}}{\text{s}^2} = \text{N}$$



$$S = \frac{5 \cdot L}{(Re_L)^{1/2}} = \frac{5(1)}{(137,000)^{1/2}} = 0.0135$$
$$= 13.5 \text{ mm}$$